

In the Claims:

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Claims 1-41 (Cancelled)

42. (Currently Amended): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H<sub>2</sub>O with employing a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of ~~comprises~~ alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m<sup>2</sup>/g impregnated with:
- (i) 0.5 to 25% by weight of an oxide of Ce, calculated as CeO<sub>2</sub>, impregnated in the support particles, and
  - (ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as CuO.

- B1
43. (Currently Amended): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H<sub>2</sub>O with employing a low-pyrophoricity water-gas shift reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of ~~comprises~~ alumina support particles with a mesh size of 12 or greater and a BET surface area of at least 10 m<sup>2</sup>/g impregnated with:
- (i) 0.5 to 25% by weight of an oxide of cerium, calculated as CeO<sub>2</sub> impregnated in the support particles;
  - (ii) 0.5 to 10% by weight of an oxide of chromium, calculated as Cr<sub>2</sub>O<sub>3</sub>, impregnated in the support particles; wherein the combined concentration of the oxides of cerium and chromium is between 0.5 to 35% by weight; and
  - (iii) between 4 and 14% by weight catalytic agent, wherein the catalytic agent is copper or an oxide thereof, calculated as CuO.

44. (Cancelled)

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- B2
45. (New): A process for carrying out the water-gas shift reaction, comprising contacting an input gas stream comprising CO and H<sub>2</sub>O with a low-pyrophoricity water-gas shift

reaction catalyst; wherein the low-pyrophoricity water-gas shift reaction catalyst consists essentially of alumina support particles with a mesh size of 12 or greater and a BET surface area of at least  $10 \text{ m}^2/\text{g}$  impregnated with:

- (i) 0.5 to 15% by weight of an oxide of chromium, calculated as  $\text{Cr}_2\text{O}_3$ , impregnated in the support particles, and
- (ii) between 4 and 14% by weight catalytic agent wherein the catalytic agent is Cu or an oxide thereof, calculated as  $\text{CuO}$ .

46. (New): The process of claim 42, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume  $\text{CO}$ ,
  - (ii) at least 10% by volume hydrogen, and
  - (iii) at least 10% by volume  $\text{H}_2\text{O}$ ; and
- wherein the input gas stream has a space velocity of at least  $500 \text{ hr}^{-1}$  VHSV.

47. (New): The process of claim 43, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume  $\text{CO}$ ,
  - (ii) at least 10% by volume hydrogen, and
  - (iii) at least 10% by volume  $\text{H}_2\text{O}$ ; and
- wherein the input gas stream has a space velocity of at least  $500 \text{ hr}^{-1}$  VHSV.

48. (New): The process of claim 45, wherein the input gas stream comprises:

- (i) between about 1% by volume and about 10% by volume  $\text{CO}$ ,
  - (ii) at least 10% by volume hydrogen, and
  - (iii) at least 10% by volume  $\text{H}_2\text{O}$ ; and
- wherein the input gas stream has a space velocity of at least  $500 \text{ hr}^{-1}$  VHSV.